

(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property
Organization
International Bureau



(10) International Publication Number
WO 2017/044365 A1

(43) International Publication Date
16 March 2017 (16.03.2017)

(51) International Patent Classification:

C01B 39/02 (2006.01) C01B 39/30 (2006.01)
C01B 39/48 (2006.01)

(21) International Application Number:

PCT/US2016/049826

(22) International Filing Date:

1 September 2016 (01.09.2016)

(25) Filing Language:

English

(26) Publication Language:

English

(30) Priority Data:

62/217,071 11 September 2015 (11.09.2015) US

(71) Applicant: CHEVRON U.S.A. INC. [US/US]; 6001
Bollinger Canyon Road, San Ramon, California 94583
(US).

(72) Inventor: XIE, Dan; 6001 Bollinger Canyon Road, San
Ramon, California 94583 (US).

(74) Agents: FLAHERTY, Terrence M. et al.; Chevron Cor-
poration, Law Department, Post Office Box 6006, San Ra-
mon, California 94583-0806 (US).

(81) Designated States (unless otherwise indicated, for every
kind of national protection available): AE, AG, AL, AM,
AO, AT, AU, AZ, BA, BB, BG, BH, BN, BR, BW, BY,
BZ, CA, CH, CL, CN, CO, CR, CU, CZ, DE, DK, DM,

DO, DZ, EC, EE, EG, ES, FI, GB, GD, GE, GH, GM, GT,
HN, HR, HU, ID, IL, IN, IR, IS, JP, KE, KG, KN, KP, KR,
KZ, LA, LC, LK, LR, LS, LU, LY, MA, MD, ME, MG,
MK, MN, MW, MX, MY, MZ, NA, NG, NI, NO, NZ, OM,
PA, PE, PG, PH, PL, PT, QA, RO, RS, RU, RW, SA, SC,
SD, SE, SG, SK, SL, SM, ST, SV, SY, TH, TJ, TM, TN,
TR, TT, TZ, UA, UG, US, UZ, VC, VN, ZA, ZM, ZW.

(84) Designated States (unless otherwise indicated, for every
kind of regional protection available): ARIPO (BW, GH,
GM, KE, LR, LS, MW, MZ, NA, RW, SD, SL, ST, SZ,
TZ, UG, ZM, ZW), Eurasian (AM, AZ, BY, KG, KZ, RU,
TJ, TM), European (AL, AT, BE, BG, CH, CY, CZ, DE,
DK, EE, ES, FI, FR, GB, GR, HR, HU, IE, IS, IT, LT, LU,
LV, MC, MK, MT, NL, NO, PL, PT, RO, RS, SE, SI, SK,
SM, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ,
GW, KM, ML, MR, NE, SN, TD, TG).

Declarations under Rule 4.17:

- as to applicant's entitlement to apply for and be granted a
patent (Rule 4.17(ii))
- as to the applicant's entitlement to claim the priority of the
earlier application (Rule 4.17(iii))

Published:

- with international search report (Art. 21(3))



WO 2017/044365 A1

(54) Title: METHOD FOR PREPARING ZEOLITE SSZ-98

(57) Abstract: A method is disclosed for preparing zeolite SSZ-98 using 1,3-dicyclohexylimidazolium cations as a structure directing agent.

METHOD FOR PREPARING ZEOLITE SSZ-98

TECHNICAL FIELD

[001] This disclosure relates generally to a method for preparing zeolite SSZ-98 using 1,3-dicyclohexylimidazolium cations as a structure directing agent.

BACKGROUND

[002] Molecular sieves are a commercially important class of crystalline materials. They have distinct crystal structures with ordered pore structures which are demonstrated by distinct X-ray diffraction patterns. The crystal structure defines cavities and pores which are characteristic of the different species.

[003] Molecular sieves are classified by the Structure Commission of the International Zeolite Association (IZA) according to the rules of the IUPAC Commission on Zeolite Nomenclature. According to this classification, framework type zeolites and other crystalline microporous molecular sieves, for which a structure has been established, are assigned a three letter code and are described in the *"Atlas of Zeolite Framework Types,"* Sixth Revised Edition, Elsevier (2007).

[004] ERI framework type materials are characterized by three-dimensional 8-membered-ring pore/channel systems containing double-six-rings (d6r) and cages. Small pore zeolites containing d6r building units and cages have shown utility in methanol-to-olefins catalysis and in the selective catalytic reduction of nitrogen oxides (NO_x) to name some of the more important commercial applications.

[005] U.S. Patent Application Publication Nos. 2016/0002059 and 2016/0002060 disclose an ERI framework type molecular sieve designated SSZ-98 and its synthesis using N,N'-dimethyl-1,4-diazabicyclo[2.2.2]octane dications as a structure directing agent.

[006] It has now been found that 1,3-dicyclohexylimidazolium cations are effective as a structure directing agent in the synthesis of SSZ-98.

SUMMARY

[007] In one aspect, there is provided a method of preparing zeolite SSZ-98 by contacting under crystallization conditions (1) at least one source of silicon oxide; (2) at least one source of aluminum oxide; (3) at least one source of a metal selected from Groups 1 and 2 of the Periodic Table; (4) 1,3-dicyclohexylimidazolium cations; and (5) hydroxide ions.

[008] In one aspect, there is provided a process for preparing zeolite SSZ-98 by: (a) preparing a reaction mixture containing: (1) at least one source of silicon oxide; (2) at least one source of aluminum oxide; (3) at least one source of a metal selected from Groups 1 and 2 of the Periodic Table; (4) 1,3-dicyclohexylimidazolium cations; (5) hydroxide ions; and (6) water; and (b) subjecting the reaction mixture to crystallization conditions sufficient to form crystals of the zeolite.

[009] In one aspect, there is provided zeolite SSZ-98 containing 1,3-dicyclohexylimidazolium cations within its pore structure.

[010] In one aspect, there is provided crystalline zeolite SSZ-98 having a composition, as-synthesized and in the anhydrous state, in terms of mole ratios, as follows:

	Broad	Exemplary
$\text{SiO}_2/\text{Al}_2\text{O}_3$	10 to 50	15 to 35
Q/SiO_2	0.02 to 0.20	0.05 to 0.20
M/SiO_2	0.01 to 0.20	0.02 to 0.15

wherein Q comprises 1,3-dicyclohexylimidazolium cations and M is selected from the group consisting of metals from Groups 1 and 2 of the Periodic Table.

DETAILED DESCRIPTION

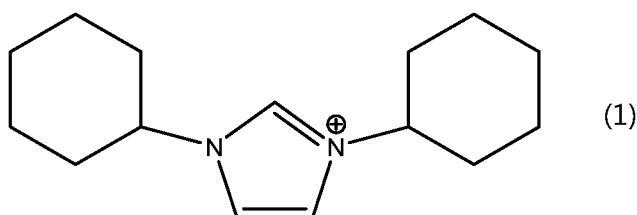
Introduction

[011] The following terms will be used throughout the specification and will have the following meanings unless otherwise indicated.

[012] The term "zeolite" refers to crystalline aluminosilicate compositions which are microporous and which are formed from corner-sharing AlO_2 and SiO_2 tetrahedra.

[013] As used herein, the numbering scheme for the Periodic Table Groups is as disclosed in *Chem. Eng. News*, 63(5), 26-27 (1985).

[014] In preparing zeolite SSZ-98, a 1,3-dicyclohexylimidazolium cation is used as a structure directing agent ("SDA"), also known as a crystallization template. The SDA useful for making SSZ-98 is represented by the following structure (1):



1,3-dicyclohexylimidazolium cation

[015] The SDA cation is associated with anions which can be any anion that is not detrimental to the formation of the zeolite. Representative anions include elements from Group 17 of the Periodic Table (e.g., fluoride, chloride, bromide, and iodide), hydroxide, sulfate, tetrafluoroborate, acetate, carboxylate, and the like.

Reaction Mixture

[016] In general, zeolite SSZ-98 is prepared by: (a) preparing a reaction mixture containing (1) at least one source of silicon oxide; (2) at least one source of aluminum oxide; (3) at least one source of a metal selected from Groups 1 and 2 of the Periodic Table; (4) 1,3-dicyclohexylimidazolium cations; (5) hydroxide ions; and (6) water; and (b) subjecting the reaction mixture to crystallization conditions sufficient to form crystals of the zeolite.

[017] The composition of the reaction mixture from which the zeolite is formed, in terms of mole ratios, is identified in Table 1 below:

TABLE 1

	Broad	Exemplary
SiO ₂ /Al ₂ O ₃	10 to 100	15 to 80
M/SiO ₂	0.05 to 0.45	0.15 to 0.40
Q/SiO ₂	0.10 to 0.80	0.15 to 0.40
OH/SiO ₂	0.20 to 1.00	0.20 to 0.60
H ₂ O/SiO ₂	10 to 80	15 to 50

wherein M is selected from the group consisting of metals from Groups 1 and 2 of the Periodic Table and Q comprises 1,3-dicyclohexylimidazolium cations.

[018] Sources useful herein for silicon oxide include fumed silica, precipitated silicates, silica hydrogel, silicic acid, colloidal silica, tetra-alkyl orthosilicates (e.g., tetraethyl orthosilicate), and silica hydroxides.

[019] Sources useful herein for aluminum oxide include aluminates, alumina, and aluminum compounds (e.g., aluminum chloride, aluminum hydroxide, and aluminum sulfate), kaolin clays, and other zeolites (e.g., zeolite Y).

[020] As described herein above, for each embodiment described herein, the reaction mixture can be formed using at least one source of a metal (M) selected from Groups 1 and 2 of the Periodic Table. In one sub-embodiment, the reaction mixture is formed using a source of a metal from Group 1 of the Periodic Table. In another sub-embodiment, the reaction mixture is formed using a source of potassium (K). Any M-containing compound which is not detrimental to the crystallization process is suitable. Sources for such Groups 1 and 2 metals include oxides, hydroxides, nitrates, sulfates, halides, acetates, oxalates and citrates thereof.

[021] Optionally, the reaction mixture may contain seed crystals. In one embodiment, synthesis of the crystalline zeolite is facilitated by the presence of 0.05 to 10.0 wt. % (e.g., 1 to 5 wt. %) seed crystals based on the total weight of the reaction mixture. The seed crystals can be isostructural with the desired zeolite, for example, the product of a previous synthesis.

[022] For each embodiment described herein, the reaction mixture can be supplied by more than one source. Also, two or more reaction components can be provided by one source.

[023] The reaction mixture can be prepared either batch wise or continuously. Crystal size, morphology and crystallization time of the crystalline zeolite described herein can vary with the nature of the reaction mixture and the crystallization conditions.

Crystallization and Post-Synthesis Treatment

[024] Crystallization of the zeolite can be carried out under either static, tumbled or stirred conditions in a suitable reactor vessel, such as for example polypropylene jars or Teflon-lined or stainless steel autoclaves, at a temperature of from 125°C to 200°C for a time sufficient for crystallization to occur at the temperature used, e.g., from 1 day to 14 days.

[025] Once the zeolite crystals have formed, the solid product is separated from the reaction mixture by standard mechanical separation techniques such as centrifugation or filtration. The crystals are water-washed and then dried to obtain the as-synthesized zeolite crystals. The drying step is typically performed at a temperature of less than 200°C.

[026] As a result of the crystallization process, the recovered crystalline zeolite product contains within its pore structure at least a portion of the structure directing agent used in the synthesis.

[027] The structure directing agent is typically at least partially removed from the zeolite by calcination before use. Calcination consists essentially of heating the zeolite comprising the structure directing agent at a temperature of from 200°C to 800°C in the presence of an oxygen-containing gas, optionally in the presence of steam. The structure directing agent can also be removed by photolysis techniques as described in U.S. Patent No. 6,960,327.

[028] To the extent desired and depending on the composition of the zeolite, any cations in the as-synthesized or calcined zeolite can be replaced in accordance with techniques well known in the art by ion exchange with other cations. Preferred replacing cations include metal ions, hydrogen ions, hydrogen precursor, e.g., ammonium ions and mixtures thereof. Particularly preferred cations are those which tailor the catalytic activity for certain hydrocarbon conversion reactions. These include hydrogen, rare earth metals and metals of Groups 2 to 15 of the Periodic Table of the Elements. As used herein, the term "as-synthesized" refers to the zeolite in its form after crystallization, prior to removal of the SDA cation.

[029] The zeolite disclosed herein can be formulated with into a catalyst composition by combination with other materials, such as binders and/or matrix materials, which provide additional hardness or catalytic activity to the finished catalyst.

Characterization of the Zeolite

[030] SSZ-98 zeolites made by the process disclosed herein have a composition (in terms of mole ratios), as-synthesized and in the anhydrous state, as described in Table 2 below:

TABLE 2

	Broad	Exemplary
$\text{SiO}_2/\text{Al}_2\text{O}_3$	10 to 50	15 to 35
Q/SiO_2	0.02 to 0.20	0.05 to 0.20
M/SiO_2	0.01 to 0.20	0.02 to 0.15

wherein Q comprises 1,3-dicyclohexylimidazolium cations and M is selected from the group consisting of metals from Groups 1 and 2 of the Periodic Table.

[031] It should be noted that the as-synthesized form of the SSZ-98 zeolite may have molar ratios different from the molar ratios of reactants of the reaction mixture used to prepare the as-synthesized form. This result may occur due to incomplete incorporation of 100% of the reactants of the reaction mixture into the crystals formed (from the reaction mixture).

[032] SSZ-98 is characterized by an X-ray diffraction pattern which, in the as-synthesized form of the zeolite, includes at least the lines set out in Table 3 below.

TABLE 3

Characteristic Peaks for As-Synthesized SSZ-98

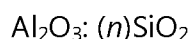
2-Theta ^(a)	<i>d</i> -spacing (nm)	Relative Intensity ^(b)
7.78	1.136	VS
9.74	0.907	W
11.79	0.750	W
13.46	0.657	S
14.10	0.627	W
15.53	0.570	M
16.62	0.533	W

19.51	0.455	W
20.56	0.432	VS
21.40	0.415	M
23.38	0.380	S
23.76	0.374	VS
24.88	0.358	W

(a) ± 0.20

(b) The powder XRD patterns provided are based on a relative intensity scale in which the strongest line in the X-ray diffraction pattern is assigned a value of 100: W = weak (> 0 to ≤ 20); M = medium (> 20 to ≤ 40); S = strong (> 40 to ≤ 60); VS = very strong (> 60 to ≤ 100).

[033] In its calcined form, the aluminosilicate SSZ-98 zeolite disclosed herein has a composition comprising the molar relationship:



wherein n has a value of from 10 to 50 (e.g., from 10 to 35, from 10 to 25, from 10 to 20, from 10 to 15, from 12 to 50, from 12 to 35, from 12 to 25, from 12 to 20, from 15 to 50, or from 15 to 35).

[034] SSZ-98 is characterized by an X-ray diffraction pattern which, in the calcined form of the zeolite, includes at least the lines set out in Table 4.

TABLE 4
Characteristic Peaks for Calcined SSZ-98

2-Theta ^(a)	d -spacing (nm)	Relative Intensity ^(b)
7.76	1.138	VS
9.78	0.904	W
11.79	0.750	W
13.45	0.658	VS
14.07	0.629	W
15.51	0.571	W
16.61	0.533	W
19.50	0.455	W
20.54	0.432	S
21.39	0.415	W
23.37	0.380	M
23.73	0.375	S
24.92	0.357	W

^(a) ± 0.20

^(b) The powder XRD patterns provided are based on a relative intensity scale in which the strongest line in the X-ray diffraction pattern is assigned a value of 100: W = weak (> 0 to ≤ 20); M = medium (> 20 to ≤ 40); S = strong (> 40 to ≤ 60); VS = very strong (> 60 to ≤ 100).

[035] Minor variations in the diffraction pattern can result from variations in the mole ratios of the framework species of the particular sample due to changes in lattice constants. In addition, sufficiently small crystals will affect the shape and intensity of peaks, leading to significant peak broadening. Minor variations in the diffraction pattern can result from variations in the organic compound used in the preparation. Calcination can also cause minor shifts in the X-ray diffraction pattern. Notwithstanding these minor perturbations, the basic crystal structure remains unchanged.

[036] The powder X-ray diffraction patterns presented herein were collected by standard techniques. The radiation was $\text{CuK}\alpha$ radiation. The peak heights and the positions, as a function of 2θ where θ is the Bragg angle, were read from the relative intensities of the peaks, and d , the interplanar spacing corresponding to the recorded lines, can be calculated.

[037] In one embodiment, zeolite SSZ-98 prepared in accordance with this disclosure is preferably substantially free of non-ERI framework type material. By "substantially free of non-ERI framework type material" is meant that the zeolite composition disclosed herein contains less than 2.5% non-ERI framework type character (e.g., less than 1% non-ERI framework type character, less than 0.5% non-ERI framework type character, or no measurable non-ERI framework type character), as measured by X-ray diffraction. The presence of these impurities can be determined and quantified by analysis of the X-ray diffraction pattern of a sample. The term "non-ERI framework type material" used herein means any material that does not contain crystalline zeolite of the ERI framework type. Examples of such non-

ERI framework type material include, for example, amorphous material and OFF framework type zeolites.

EXAMPLES

[038] The following illustrative examples are intended to be non-limiting.

EXAMPLE 1

[039] 0.78 g of 45% KOH solution and 1.00 g of CBV720 Y zeolite (Zeolyst International, $\text{SiO}_2/\text{Al}_2\text{O}_3$ mole ratio = 30) were mixed together in a Teflon liner. Then, 5.86 g of 10% 1,3-dicyclohexylimidazolium hydroxide solution (SACHEM Inc.) was added to the mixture. The resulting gel was stirred until it became homogeneous. The liner was capped and placed within a Parr steel autoclave reactor. The autoclave was placed in an oven and heated at 135°C for 5 days. The solid products were recovered from the cooled reactor by centrifugation, washed with deionized water and dried at 95°C.

[040] The resulting product was identified by powder XRD and SEM to be pure SSZ-98 zeolite.

[041] The product had a $\text{SiO}_2/\text{Al}_2\text{O}_3$ mole ratio of 12.2, as determined by ICP elemental analysis.

EXAMPLE 2

[042] 1.61 g of 45% KOH solution and 2.00 g of CBV760 Y-zeolite (Zeolyst International, $\text{SiO}_2/\text{Al}_2\text{O}_3$ mole ratio = 60) were mixed together in a Teflon liner. Then, 20.17 g of 10% 1,3-dicyclohexylimidazolium hydroxide solution (SACHEM Inc.) was added to the mixture. The resulting gel was stirred until it became homogeneous. The liner was capped and placed within a Parr steel autoclave reactor. The autoclave was placed in an oven and heated at 135°C for 6 days. The solid products were recovered from the cooled reactor by centrifugation, washed with deionized water and dried at 95°C.

[043] The resulting product was identified by powder XRD and SEM to be pure SSZ-98 zeolite.

[044] The product had a $\text{SiO}_2/\text{Al}_2\text{O}_3$ mole ratio of 14.5, as determined by ICP elemental analysis.

EXAMPLE 3

[045] 1.81 g of 45% KOH solution and 2.00 g of CBV780 Y-zeolite (Zeolyst International, $\text{SiO}_2/\text{Al}_2\text{O}_3$ mole ratio = 80) were mixed together in a Teflon liner. Then, 12.10 g of 10% 1,3-dicyclohexylimidazolium hydroxide solution (SACHEM Inc.) was added to the mixture. The resulting gel was stirred until it became homogeneous. The liner was capped and placed within a Parr steel autoclave reactor. The autoclave was placed in an oven and heated at 135°C for 6 days. The solid products were recovered from the cooled reactor by centrifugation, washed with deionized water and dried at 95°C.

[046] The resulting product was identified by powder XRD and SEM to be pure SSZ-98 zeolite.

[047] The product had a $\text{SiO}_2/\text{Al}_2\text{O}_3$ mole ratio of 15.2, as determined by ICP elemental analysis.

[048] As used herein, the term "comprising" means including elements or steps that are identified following that term, but any such elements or steps are not exhaustive, and an embodiment can include other elements or steps.

[049] Unless otherwise specified, the recitation of a genus of elements, materials or other components, from which an individual component or mixture of components can be selected, is intended to include all possible sub-generic combinations of the listed components and mixtures thereof.

[050] All documents cited in this application are herein incorporated by reference in their entirety to the extent such disclosure is not inconsistent with this text.

CLAIMS

1. A method of preparing zeolite SSZ-98, comprising:
- (a) preparing a reaction mixture containing:
- (1) at least one source of silicon oxide;
 - (2) at least one source of aluminum oxide;
 - (3) at least one source of a metal (M) selected from Groups 1 and 2 of the Periodic Table;
 - (4) 1,3-dicyclohexylimidazolium cations (Q);
 - (5) hydroxide ions; and
 - (6) water; and
- (b) subjecting the reaction mixture to crystallization condition sufficient to form crystals of the zeolite.

2. The method of claim 1, wherein the zeolite is prepared from a reaction mixture comprising, in terms of mole ratios, the following:

$\text{SiO}_2/\text{Al}_2\text{O}_3$	10 to 100
M/SiO_2	0.05 to 0.45
Q/SiO_2	0.10 to 0.80
OH/SiO_2	0.20 to 1.00
$\text{H}_2\text{O}/\text{SiO}_2$	10 to 80

3. The method of claim 1, wherein the zeolite is prepared from a reaction comprising, in terms of mole ratios, the following:

$\text{SiO}_2/\text{Al}_2\text{O}_3$	15 to 80
M/SiO_2	0.15 to 0.40
Q/SiO_2	0.15 to 0.40
OH/SiO_2	0.20 to 0.60
$\text{H}_2\text{O}/\text{SiO}_2$	15 to 50

4. The method of claim 1, wherein the zeolite has a composition, as-synthesized and in the anhydrous state, in terms of mole ratios, as follows:

$\text{SiO}_2/\text{Al}_2\text{O}_3$	10 to 50
--------------------------------------	----------

Q/SiO ₂	0.02 to 0.20
M/SiO ₂	0.01 to 0.20

5. The method of claim 1, wherein the zeolite has a composition, as-synthesized and in the anhydrous state, in terms of mole ratios, as follows:

SiO ₂ /Al ₂ O ₃	15 to 35
Q/SiO ₂	0.05 to 0.20
M/SiO ₂	0.02 to 0.15

6. The method of claim 1, wherein the zeolite has, in its as-synthesized form, an X-ray diffraction pattern including the following lines:

2-Theta	<i>d</i> -spacing (nm)	Relative Intensity
7.78 ± 0.20	1.136	VS
9.74 ± 0.20	0.907	W
11.79 ± 0.20	0.750	W
13.46 ± 0.20	0.657	S
14.10 ± 0.20	0.627	W
15.53 ± 0.20	0.570	M
16.62 ± 0.20	0.533	W
19.51 ± 0.20	0.455	W
20.56 ± 0.20	0.432	VS
21.40 ± 0.20	0.415	M
23.38 ± 0.20	0.380	S
23.76 ± 0.20	0.374	VS
24.88 ± 0.20	0.358	W

7. An SSZ-98 zeolite comprising 1,3-dicyclohexylimidazolium cations within its pore structure.

8. The zeolite of claim 7, wherein the zeolite has a SiO₂/Al₂O₃ mole ratio of from 10 to 50.

9. The zeolite of claim 7, wherein the zeolite has a SiO₂/Al₂O₃ mole ratio of from 10 to 35.

10. The zeolite of claim 7, having, in its as-synthesized form, an X-ray diffraction pattern including the following lines:

2-Theta	<i>d</i> -spacing (nm)	Relative Intensity
7.78 ± 0.20	1.136	VS
9.74 ± 0.20	0.907	W
11.79 ± 0.20	0.750	W
13.46 ± 0.20	0.657	S
14.10 ± 0.20	0.627	W
15.53 ± 0.20	0.570	M
16.62 ± 0.20	0.533	W
19.51 ± 0.20	0.455	W
20.56 ± 0.20	0.432	VS
21.40 ± 0.20	0.415	M
23.38 ± 0.20	0.380	S
23.76 ± 0.20	0.374	VS
24.88 ± 0.20	0.358	W

INTERNATIONAL SEARCH REPORT

International application No
PCT/US2016/049826

A. CLASSIFICATION OF SUBJECT MATTER
INV. C01B39/02 C01B39/48 C01B39/30
ADD.
According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED
Minimum documentation searched (classification system followed by classification symbols)
C01B
Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)
EPO-Internal, COMPENDEX, INSPEC, WPI Data

C. DOCUMENTS CONSIDERED TO BE RELEVANT		
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	US 2006/073094 A1 (MILLER MARK A [US] ET AL) 6 April 2006 (2006-04-06) paragraph [0006]; example 1 the whole document	1-10
A	US 2010/260665 A1 (ARCHER RAYMOND [US] ET AL) 14 October 2010 (2010-10-14) paragraph [0062]; claims 3,22,23,58,71; tables 4,8,10 the whole document	1-10

Further documents are listed in the continuation of Box C.

See patent family annex.

* Special categories of cited documents :

- "A" document defining the general state of the art which is not considered to be of particular relevance
- "E" earlier application or patent but published on or after the international filing date
- "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- "O" document referring to an oral disclosure, use, exhibition or other means
- "P" document published prior to the international filing date but later than the priority date claimed

- "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
- "X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
- "Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
- "&" document member of the same patent family

Date of the actual completion of the international search 21 October 2016	Date of mailing of the international search report 31/10/2016
---	---

Name and mailing address of the ISA/ European Patent Office, P.B. 5818 Patentlaan 2 NL - 2280 HV Rijswijk Tel. (+31-70) 340-2040, Fax: (+31-70) 340-3016	Authorized officer Follens, Lana
--	--

INTERNATIONAL SEARCH REPORT

Information on patent family members

International application No

PCT/US2016/049826

Patent document cited in search report	Publication date	Patent family member(s)	Publication date	
US 2006073094	A1	06-04-2006	CN 101072728 A	14-11-2007
			EP 1797005 A2	20-06-2007
			JP 5498658 B2	21-05-2014
			JP 2008515760 A	15-05-2008
			RU 2377181 C2	27-12-2009
			US 2006073094 A1	06-04-2006
			WO 2006137900 A2	28-12-2006

US 2010260665	A1	14-10-2010	AU 2010233109 A1	13-10-2011
			CA 2757854 A1	14-10-2010
			CN 102387992 A	21-03-2012
			EP 2417061 A2	15-02-2012
			JP 5908395 B2	26-04-2016
			JP 2012523367 A	04-10-2012
			JP 2016128385 A	14-07-2016
			KR 20120000577 A	02-01-2012
			US 2010260665 A1	14-10-2010
			US 2014093448 A1	03-04-2014
			US 2016272503 A1	22-09-2016
			WO 2010118377 A2	14-10-2010
ZA 201107010 B	27-12-2012			
